



# 2008 International ANSYS Conference

## Vaporization Model for Solid Agent Contaminated Charcoal

Yunhan Zheng, Ph.D.  
Research Engineer  
Continental Research and Engineering

# Vaporization Model for Solid Agent Contaminated Charcoal



## About Continental Research and Engineering, LLC

Continental Research and Engineering (CR&E) is well known in the demilitarization industry for providing, design/research engineering, laboratory and field testing, process numerical modeling, project management, new technology research and testing, and providing solution to processing problems.



## Demilitarization Technologies

- Reverse disassembly of munitions
- Thermal treatment of liquid agents
- Thermal treatment of explosive components
- Thermally decontaminate metal parts at 1000°F for 15 minutes.
- Technologies required for decontamination / destruction of secondary and closure wastes

## Agent Contaminated Charcoal

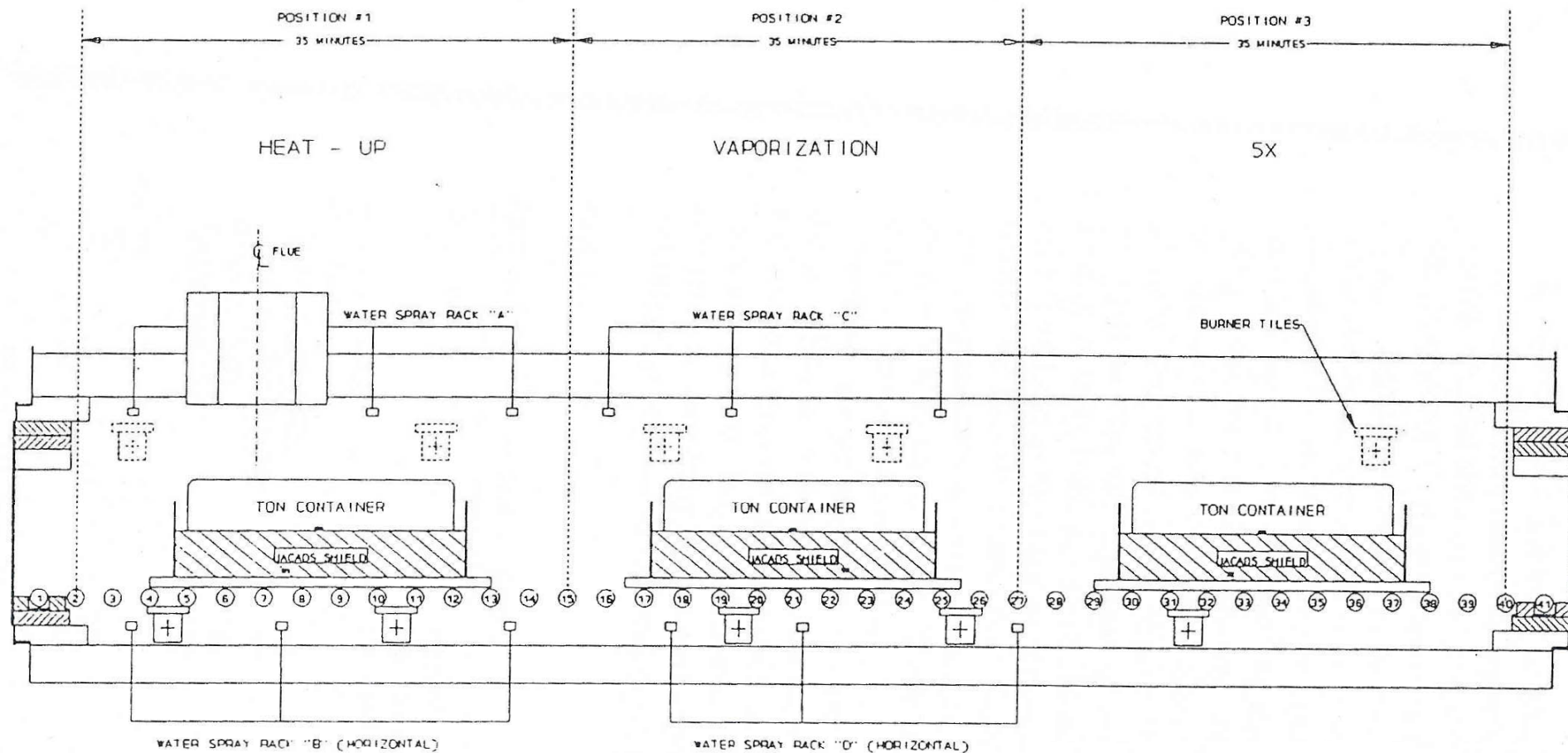
Activated charcoal used in the following process is considered secondary waste:

- As a filter for chemical agent
- Agent collection system filters
- Heating, ventilation, and air conditioning (HVAC) filters
- Pollution abatement system filtration

# Vaporization Model for Solid Agent Contaminated Charcoal



## Problem Description



# Vaporization Model for Solid Agent Contaminated Charcoal



Test one – Verify normal secondary waste process times used to 5X the charcoal. 4/28/2008

Test two – Identify extended processing time required to burn the charcoal to ash. 4/29/2008

## Objective

The contaminated charcoal heats up to 1000 °F very quickly while it continues to burn for an extended period of time. This study is to determine the heating process of different chemical agent contaminated charcoal to achieve 5X decontamination.

- Developing general vaporization model for heating process with melting/vaporization control code using dynamic moving mesh
- Calibrating the vaporization model with test data and CR&E Peak Vaporization Rate (PVR) model
- Using calibrated CFD model to predict the heating process of different chemical agent contaminated charcoal

## Vaporization Model

Fluent CFD coupled with melting/vaporization control code using dynamic moving mesh

- k- $\epsilon$  turbulence model
- Discrete Ordinates (DO) radiation model
- Melting/vaporization control UDF
- Dynamic moving mesh

## Melting and Vaporization Control UDF

Two scalars are used in the vaporization control code

First scalar - to measure the solid agent mass fraction

- Solid begins to melt when temperature of a computational cell reaches melting point
- Calculating the cell heat flux and adjust the solid mass fraction according to melting/vaporization equation
- Adjust the energy source term and momentum source term

Second scalar - to measure the liquid mass agent fraction

$$\frac{d(\rho \nabla_{cell} \epsilon_{cell})}{dt} = -\frac{Q_{cell}}{L}$$

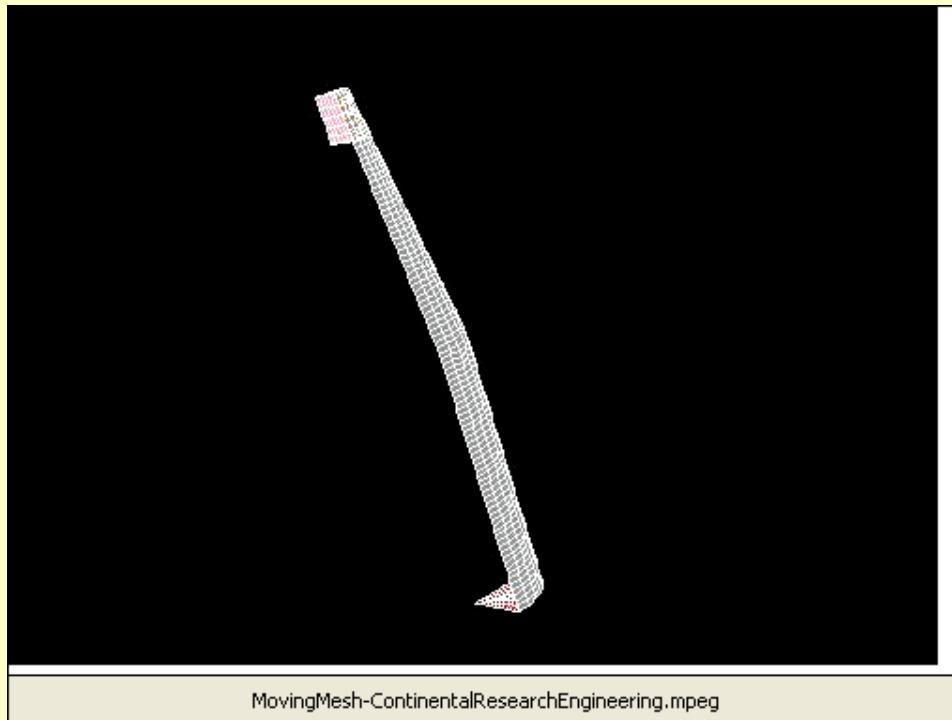
## Dynamic Moving Mesh

- DEFINE\_EXECUTE\_AT\_END and DEFINE\_GRID\_MOTION were used to control the behavior of the dynamic moving mesh during the chemical agent vaporization
- The dynamic moving mesh was based on the total heat flux of cells, current time step, latent heat of chemical agent, density of chemical agent, dimension of munitions
- Next slide shows an example of dynamic moving mesh animation of a quarter munitions

# Vaporization Model for Solid Agent Contaminated Charcoal



## Dynamic Moving Mesh



Double click to see moving mesh animation

## CR&E PVR Model

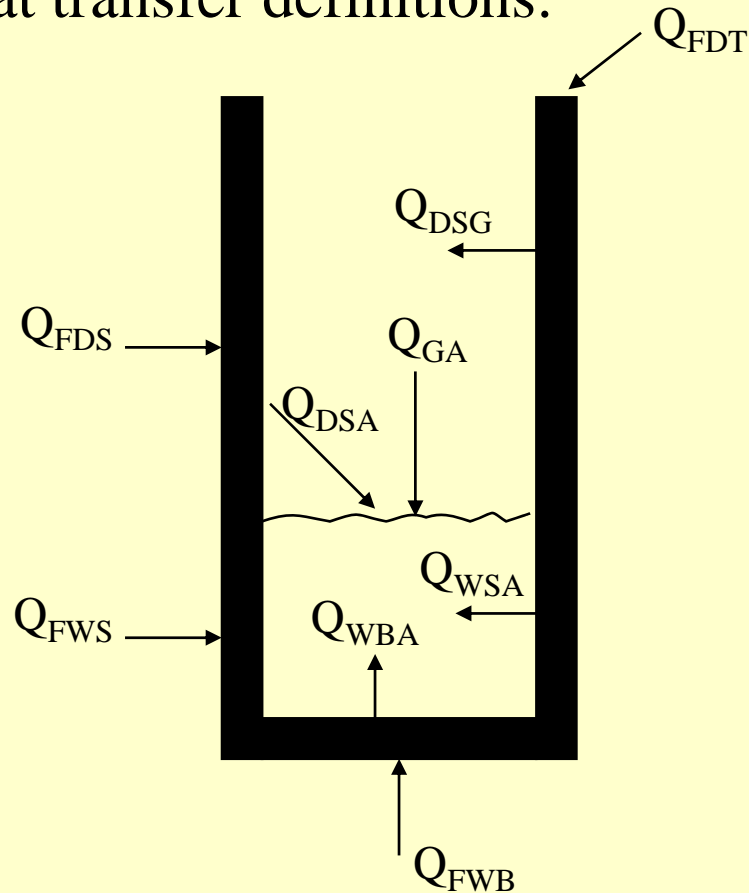
- CR&E PVR model for chemical agents GB, VX, HD and their simulants from drained projectiles on a full standard tray was developed in 1988
- The PVR program was updated and calibrated to test data in 1994.
- The PVR model is based on the munitions family groups and radiation view factor. So the model only can be used for specific munitions family

# Vaporization Model for Solid Agent Contaminated Charcoal



## CR&E PVR Model

Heat transfer definitions:



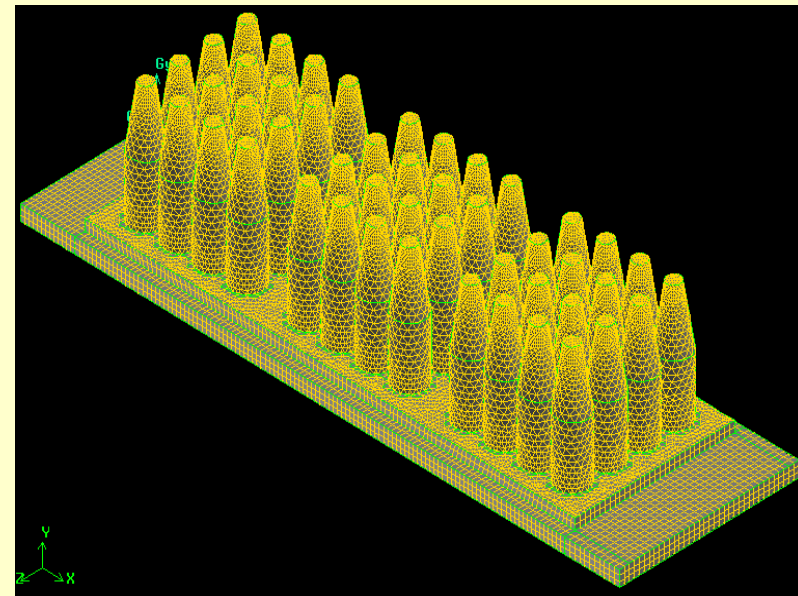
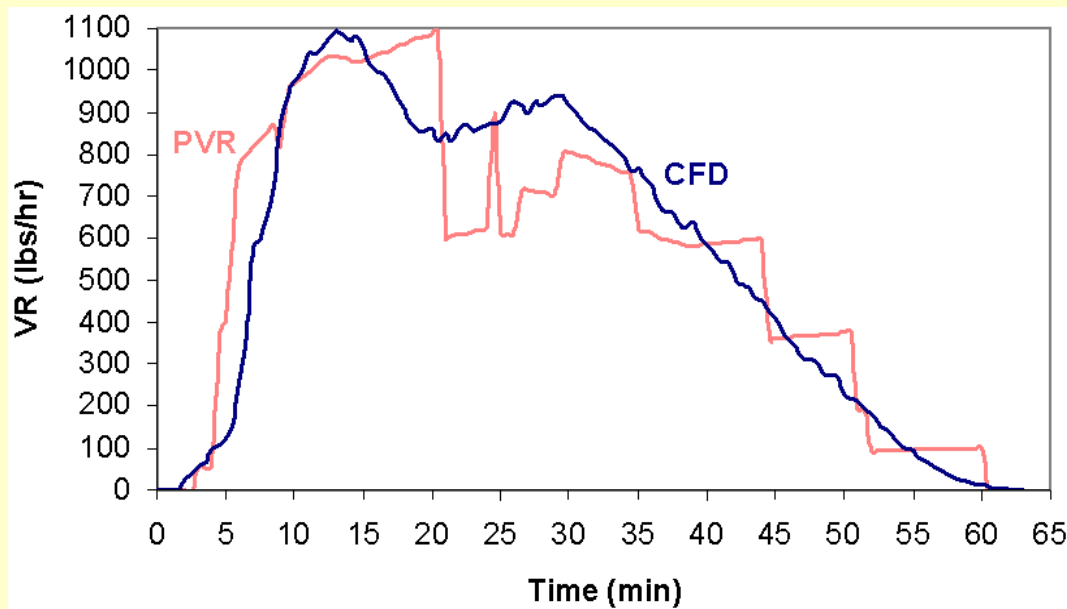
- $Q_{FDT}$  – Furnace to Dry Top
- $Q_{FDS}$  – Furnace to Dry Sides
- $Q_{FWS}$  – Furnace to Wet Sides
- $Q_{FWB}$  – Furnace to Wet Bottom
- $Q_{DSA}$  – Dry Side to Agent
- $Q_{DSG}$  – Dry Side to Gas
- $Q_{GA}$  – Gas to Agent
- $Q_{WBA}$  – Wet Bottom to Agent
- $Q_{WSA}$  – Wet side to Agent

# Vaporization Model for Solid Agent Contaminated Charcoal



## Model Calibration

(1) Munition vaporization model - the model has been verified accurate based on empirical data gathered during testing at the demilitarization facilities.



### 4.2 inch 100% Liquid HD Vaporization Rate Results

# Vaporization Model for Solid Agent Contaminated Charcoal

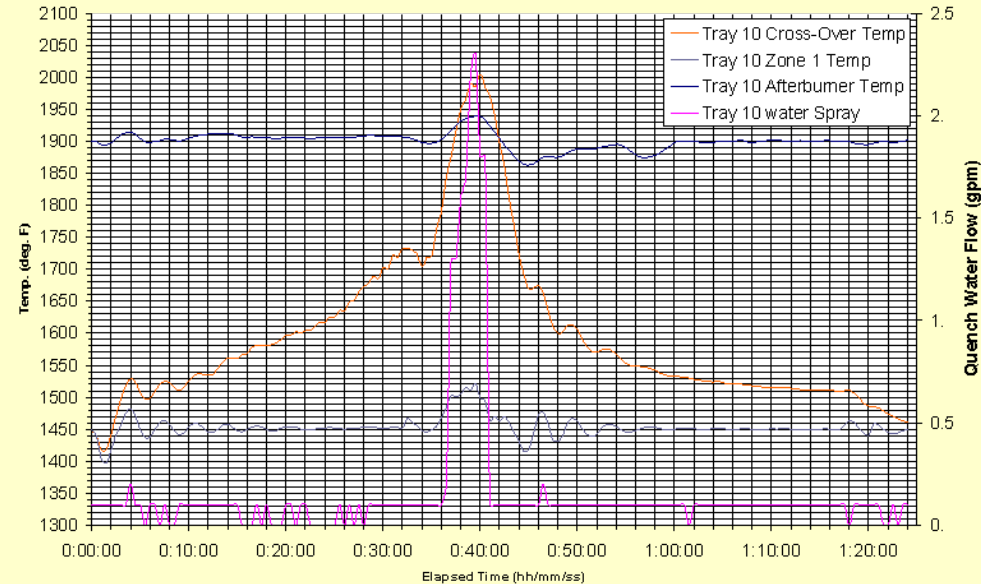


## Model Calibration

(2) Ton Container vaporization model - 45 lbm VX ton container

| Tray No. | Vap. Start Time (min) | Peak Vaporization time (min) |
|----------|-----------------------|------------------------------|
| 2        | 22:30                 | 37:30                        |
| 3        | 21:00                 | 40:30                        |
| 4        | 19:00                 | 40:00                        |
| 5        | 19:30                 | 37:30                        |
| 6        | 18:30                 | 41:00                        |
| 7        | 24:00                 | 34:30                        |
| 8        | 19:00                 | 40:00                        |
| 9        | 22:30                 | 43:30                        |
| 10       | 20:00                 | 39:30                        |
| 11       | 23:30                 | 41:00                        |
| Average  | 21:00                 | 39.30                        |

Processing Data of March 13, 2004



|            | Vap. Start Time (min) | PVR time (min) | Vap. End Time (min) |
|------------|-----------------------|----------------|---------------------|
| TOCDF data | 21:00                 | 39:30          |                     |
| PVR model  | 20:00                 | 32:00          | 43:00               |
| CFD model  | 23:00                 | 35:00          | 41:00               |

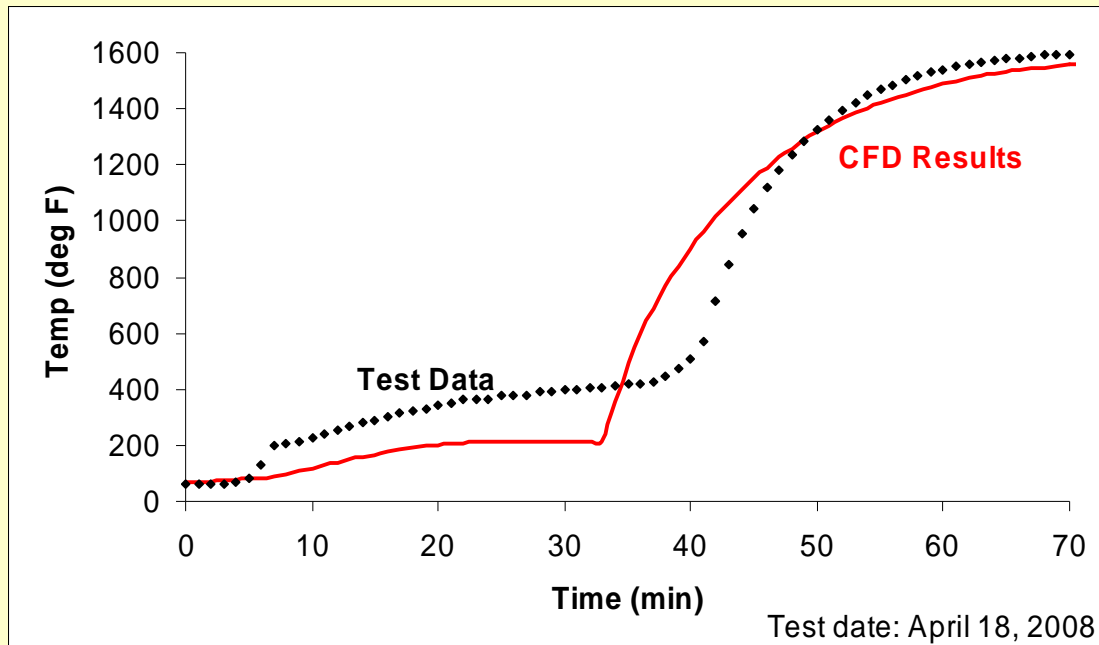
# Vaporization Model for Solid Agent Contaminated Charcoal



## Model Calibration

### (3) Wet Charcoal Heating Process Model -

- 2inx6inx6in charcoal test tray
- 23 oz charcoal
- 18 oz total water adsorbed by the charcoal
- Kiln temperature 1600 °F



## Model Application

The vaporization model with dynamic mesh has been successfully used in the processing wastes (liquid, solid, or liquid-solid mixture) through the Metal Part Furnace including the following wastes:

- Chemical warfare agents (HD, GB, VX)
- DPE suits
- Sludge
- VX hydrolysate
- Scrabbled concrete
- Secondary and closure waste
- Contaminated charcoal

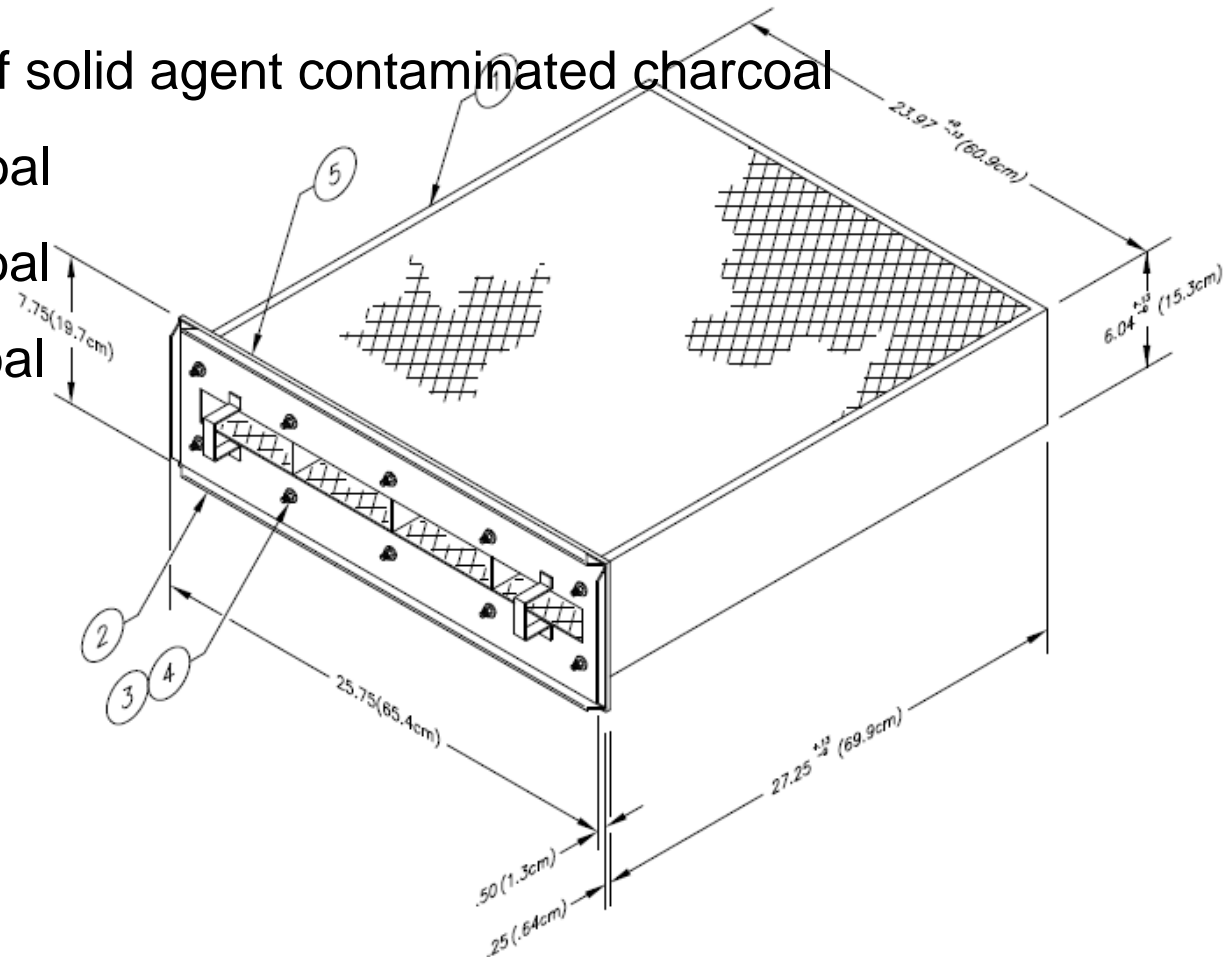
# Vaporization Model for Solid Agent Contaminated Charcoal



## Solid Agent Contaminated Charcoal

Vaporization model results of solid agent contaminated charcoal

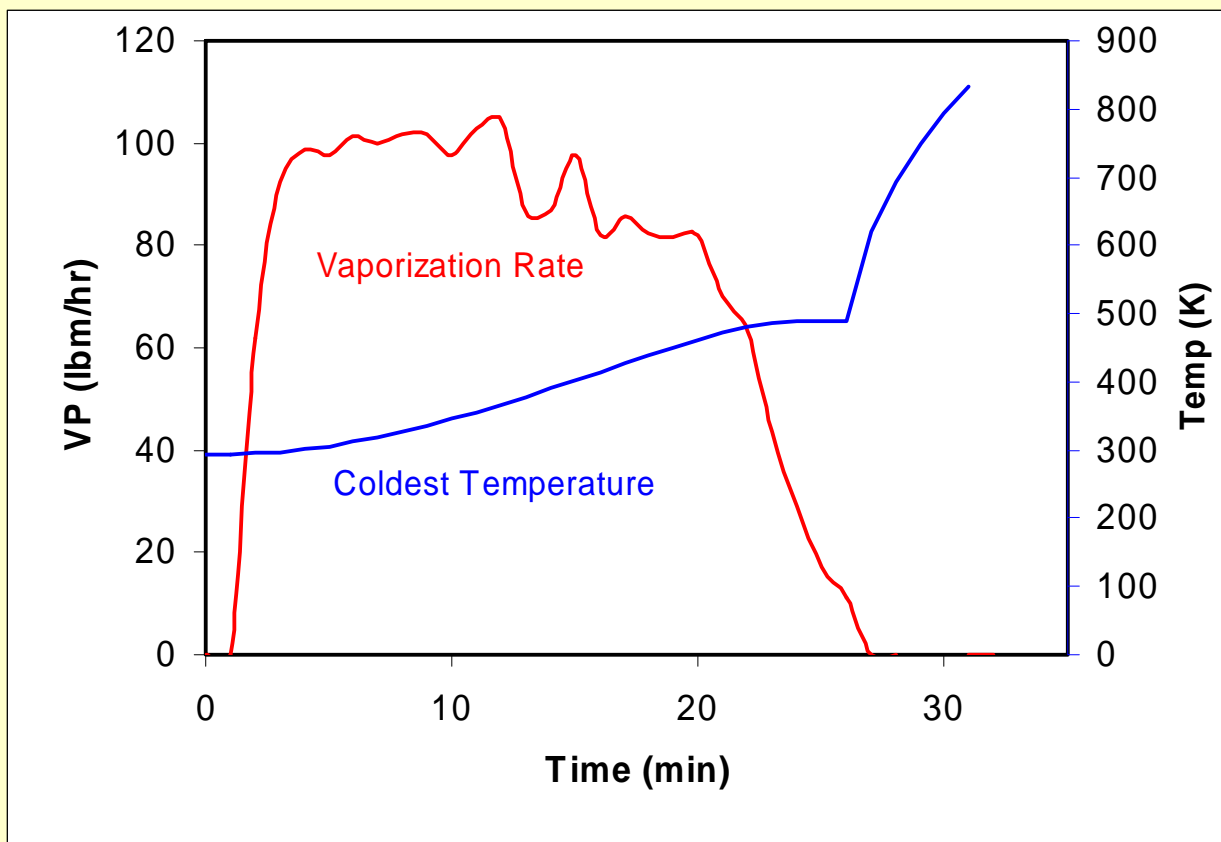
- HD contaminated charcoal
- GB contaminated charcoal
- VX contaminated charcoal



# Vaporization Model for Solid Agent Contaminated Charcoal



## Vaporization Model Results

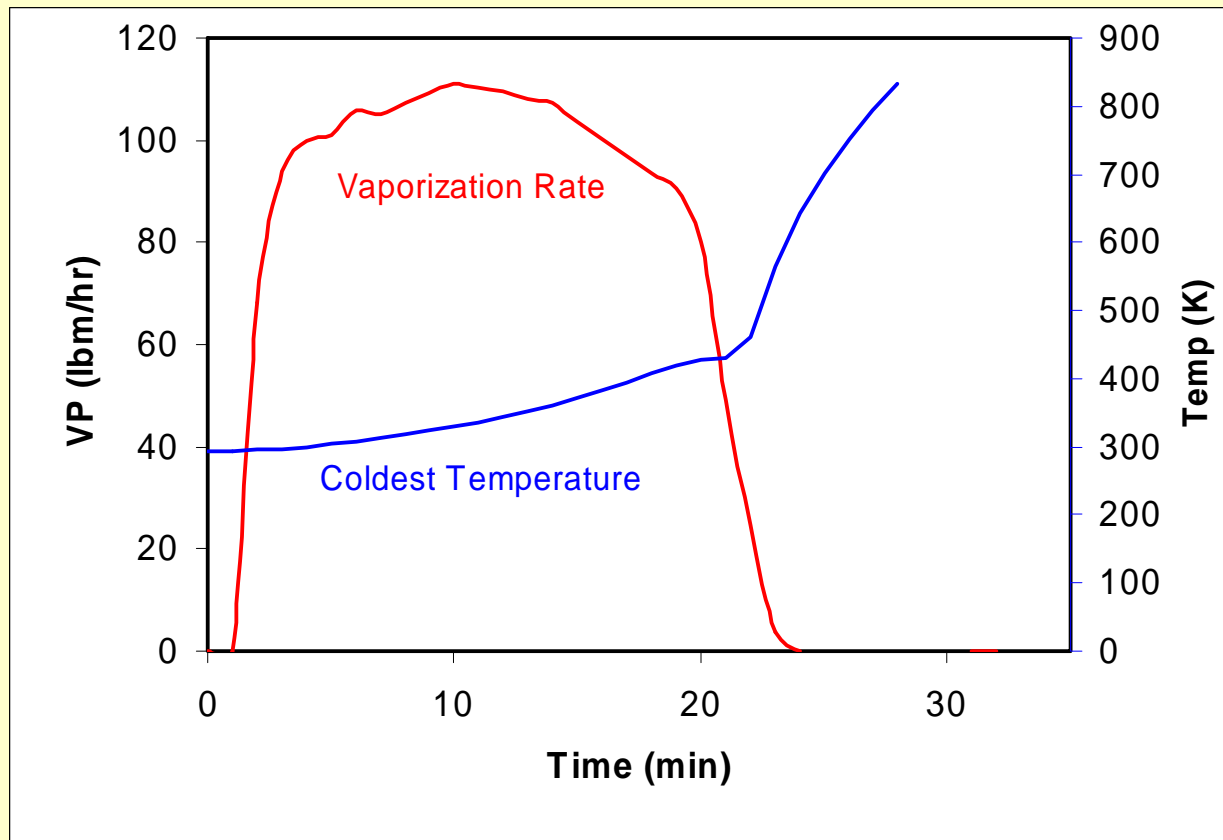


Vaporization Rate and Coldest Temperature Curve of 33 lb Agent HD with 50 lb Charcoal

# Vaporization Model for Solid Agent Contaminated Charcoal



## Vaporization Model Results

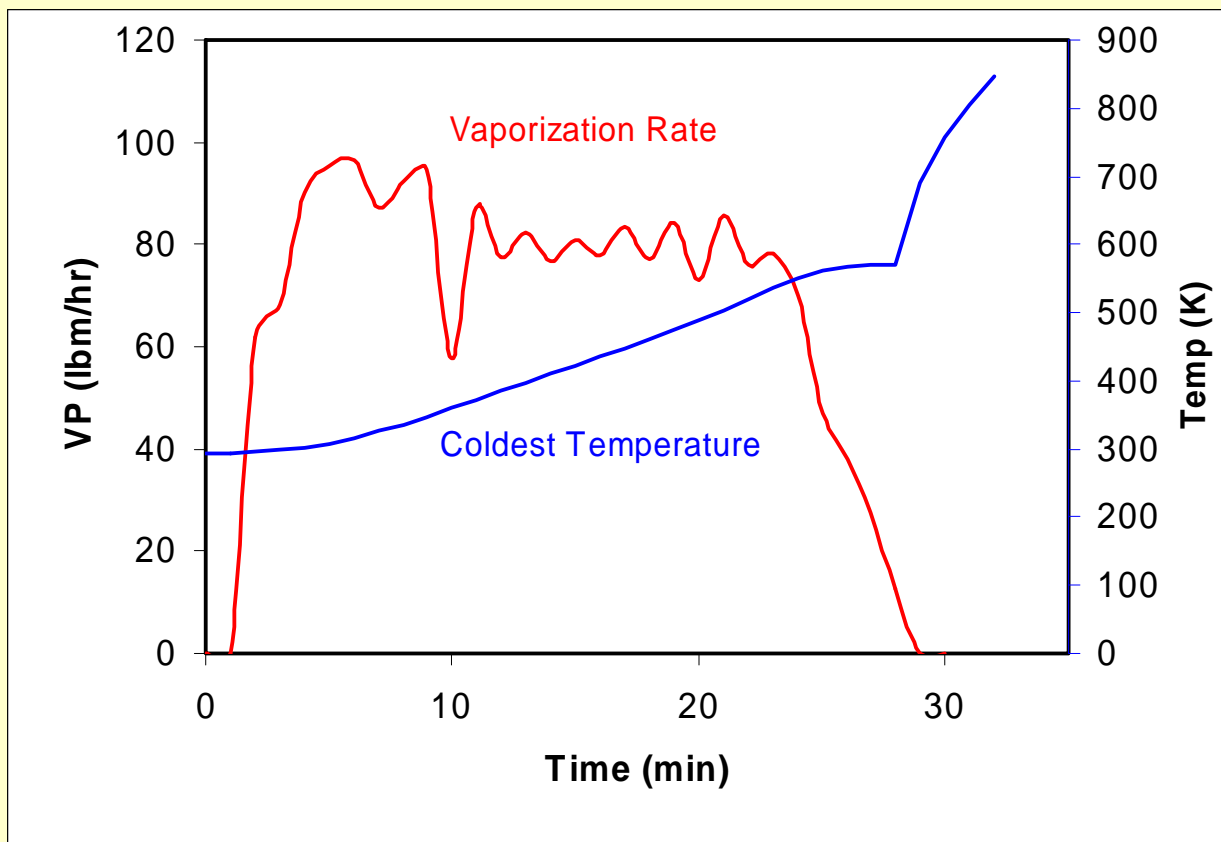


Vaporization Rate and Coldest Temperature Curve of 33 lb Agent GB with 50 lb Charcoal

# Vaporization Model for Solid Agent Contaminated Charcoal



## Vaporization Model Results



Vaporization Rate and Coldest Temperature Curve of 33 lb Agent VX with 50 lb Charcoal

## Conclusion

1. CFD model coupled with melting/vaporization code using dynamic moving mesh has been developed.
2. The vaporization model was calibrated by test data and CR&E PVR model. The predicted vaporization model results were in good agreement with PVR model results and test data.
3. This calibrated melting/vaporization dynamic model can simulate heating processing of any liquid, solid, and liquid-solid mixture. The model results have provided a guide for disposal of chemical wastes.

## Contaminated Charcoal Solution

Chemical warfare agent contaminated charcoal decontamination / destruction has been problematic

- Charcoal micronization / incineration utilized in 2000. High cost, high maintenance, problematic operation.
- Complete incineration in filter casings requires very long residence times.
- Test data and CFD model show that heating the charcoal to 1000 °F for 15 minutes utilizing existing thermal treatment system is a cost effective, simple solution for a complex problem.

## Acknowledgement

The information contained in this document is proprietary to Continental Research and Engineering, LLC. I would like to acknowledge Alfred G. Webster, CEO of Continental Research and Engineering, and Mike Vanoni, Director of operations Denver office.

*Thank You*